

# INTEGRATING RENEWABLE ENERGY SOURCES INTO ENERGY SYSTEMS FOR THE REDUCTION OF CARBON FOOTPRINTS

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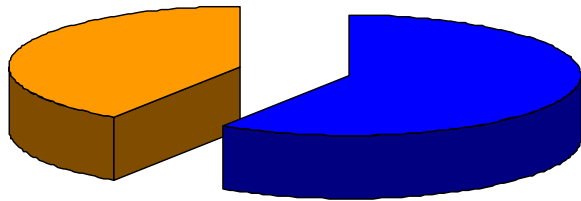
University of Pannonia

Veszprém, Hungary



## Domestic Sector Energy Use

Domestic sector



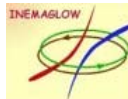
Other sectors

The domestic sector is responsible for around 30 % to 50 % of all energy use. This contributes considerably towards CO<sub>2</sub> production and should be assessed by LCA to determine its **Carbon Footprint (CFP)**

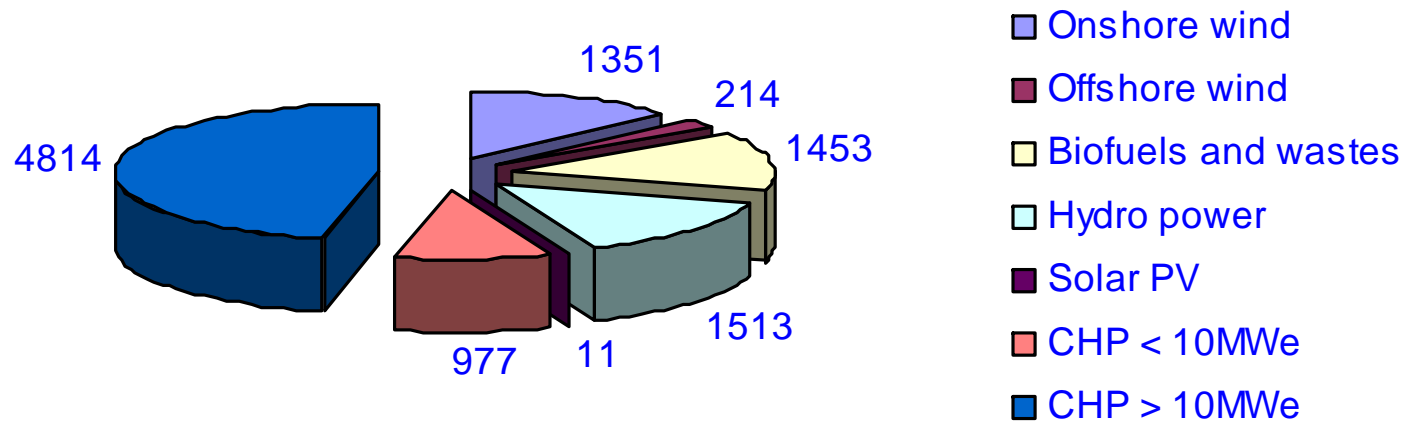
# Domestic Sector Carbon Footprint



**Carbon Footprint** is defined as the total amount of CO<sub>2</sub> and other greenhouse gases emitted over the full life cycle of a process or product.



# Technologies and their CFPs



## Current Capacity of CHP and Renewable Generation in UK [MW]

*Meeting the Energy Challenge A White Paper on Energy, May 2007  
Department of Trade and Industry, UK*

# μCHP



| <b>Annual reduction in CO<sub>2</sub> emissions</b>                                  | <b>[kgCO<sub>2</sub>]</b> |
|--|---------------------------|
| Stirling engine – unrestricted thermal surplus<br>(1 kW system)                      | - 145 (+3%)               |
| Stirling engine – restricted thermal surplus<br>(1 kW system)                        | + 574 (-10%)              |
| Stirling engine – restricted thermal surplus and<br>part-load capacity (1 kW system) | + 512 (-9%)               |
| Fuel cell (1 kW)   | + 892 (-16%)              |
| Fuel cell (3 kW)   | + 2247 (-40%)             |

*A.D Peacock., M. Newborough: Impact of micro-CHP systems on domestic sector CO<sub>2</sub> emissions, Applied Thermal Engineering 25, 2005, 2653–2676*

*Vollrad Kuhn, Jiří Klemeš, Igor Bulatov: MicroCHP: Overview of selected technologies, products and field test results, Applied Thermal Engineering, 28 (16), November 2008, 2039-2048*



# Biomass



In the UK, the carbon footprint of biomass can vary widely depending on the kind of the feedstock:  
25 gCO<sub>2</sub>/kWh (high-density wood gasification) to  
93 gCO<sub>2</sub>/kWh (combustion of low density miscanthus).

*Parliamentary Office for Science and Technology (POST), 2006. Carbon Footprint of Electricity Generation*



## Contribution to CFP in gCO<sub>2</sub>/kWh primary energy

| Origin of biomass   | Germany   | Baltic    | Sweden    | Russia    | Canada    |
|---------------------|-----------|-----------|-----------|-----------|-----------|
| Palletising         | 11        | 13        | 15        | 20        | 13        |
| Local transport     | 1         | 1         | 2         | 2         | 2         |
| Sea/River transport | 4         | 6         | 5         | 7         | 15        |
| River transport     | 2         | 2         | 2         | 2         | 2         |
| <b>TOTAL</b>        | <b>18</b> | <b>22</b> | <b>24</b> | <b>31</b> | <b>32</b> |

*Ryckmans Y. 2007. Biomass sustainability certification in Belgium, presentation at IEA Bioenergy Task 40 and EUBIONET 2 Joint Workshop, Rotterdam, The Netherlands*



## Solar



For building integrated PV systems, the total LC emissions of CO<sub>2</sub> are between 13 - 731g CO<sub>2</sub> per kWh produced (depending mainly on PV cell technology). Life cycle CO<sub>2</sub> emissions for UK PV power systems are currently 58 gCO<sub>2</sub>eq/kWh.

*NB Dependent on the geographical location: in South European countries, the CFP can be about 35gCO<sub>2</sub>eq/kWh, due to more sunlight, longer operating hours and higher energy output*

[www.nei.org/index.asp?catnum=2&catid=260](http://www.nei.org/index.asp?catnum=2&catid=260), accessed 12/09/2008





## Wind

Wind generated electricity has one of the lowest CFPs. Manufacturing and construction account for almost all of the carbon emissions, the rest being maintenance. In the UK, a typical wind generation CFP is about 4.64 gCO<sub>2</sub>eq/kWh. The availability should be also taken into consideration, and in most cases is rarely above 20 - 30 %. Back-up systems increase the effective CFP.



*Parliamentary Office for Science and Technology (POST), 2006. Carbon Footprint of Electricity Generation*

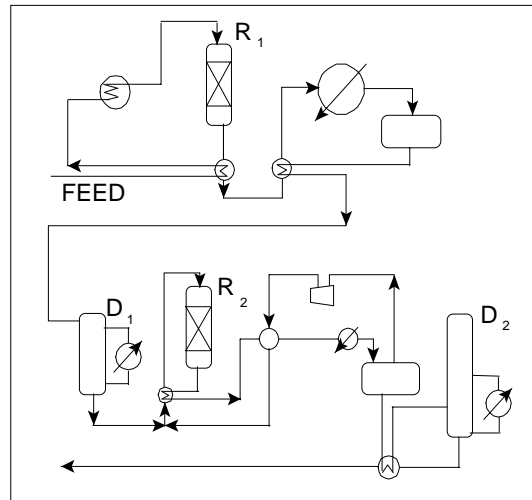


# CFPs of the some technologies

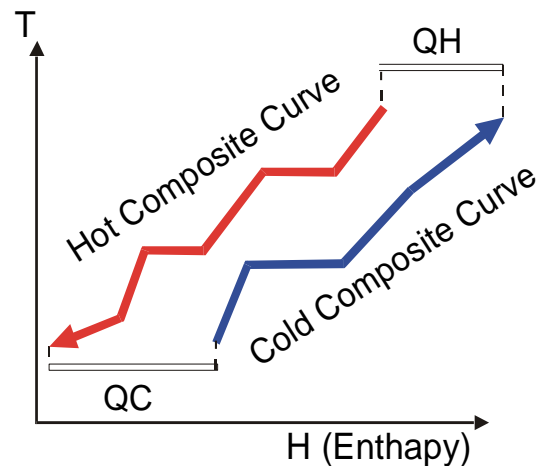
| Technology       | CFP<br>[gCO <sub>2</sub> eq/kWh]        | Factors   |
|------------------|---|---|
| Coal large scale | <b>790 - 830</b>                        | Power station type, coal quality, distance from the source, mine type, efficiency, emission treatment   |
| Gas large scale  | <b>400 - 420</b>                        | Power station type, distance from the source of gas, gas extraction, efficiency, emission treatment   |
| μCHP gas         | <b>200 - 250</b>                        | Materials used, type of CHP and its efficiency, type of fuel, distance from the manufacturer, maintenance   |
| Biomass          | <b>25 - 93</b>                          | Distance from the source of biomass, type of the transport used, type of biomass, type of combustions process, its efficiency, emission (e.g. NO <sub>x</sub> ) treatment |
| Solar            | <b>30 – 80</b><br>(backup not included) | Geographical location to sun, distance from the manufacturer, type of Solar Cells and their efficiency, materials used, maintenance needed, backup                        |
| Wind             | <b>2 – 8</b><br>(backup not included)   | Location related to wind, place of installation, distance to the manufacturer, maintenance needed related to the environment, back-up                                     |



# Existing Process Integrating Technologies



Process Integration is a long-established technology initially developed (Centre for Process Integration, The University of Manchester) for single process analysis, design and understanding



*Linnhoff, B. and D. R. Vredeveld, 1984, Pinch Technology has Come of Age, Chemical Engineering Progress, July 1984, 33-40.*



## Existing Process Integrating Technologies (Cont.)

It was further developed bringing in new concepts and methodologies have combined thermodynamics and mathematical modelling into an integrated systematic approach to the design and analysis of small and large energy based systems.

*Klemeš, J., V. R. Dhole, K. Raissi, S.J. Perry and L. Puigjaner, 1997, Targeting and Design Methodology for Reduction of Fuel, Power and CO2 on Total Sites, Applied Thermal Engineering, 17, 993 - 1003*

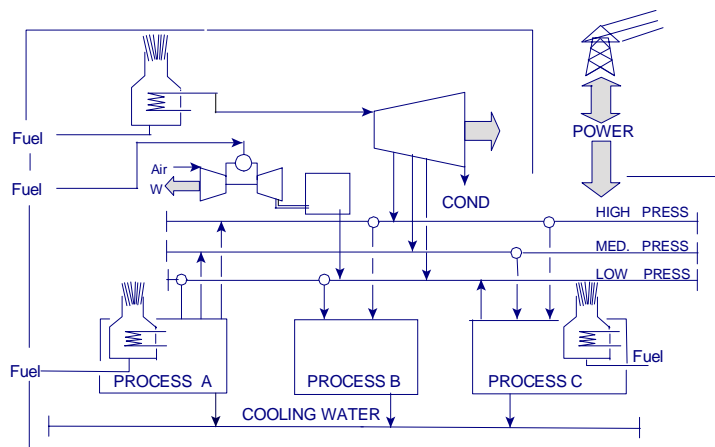
*Varbanov, P., S. Doyle and R. Smith, 2004, Modelling and Optimisation of Utility Systems, Chemical Engineering Research and Design, 82, 561-578.*

*Varbanov, P., S. Perry, Y. Makwana, X X Zhu and R. Smith, 2004, Top-Level Analysis of Site Utility Systems, Chemical Engineering Research and Design, 82(A6), 784-795.*

*Varbanov, P., S. Perry, J. Klemeš and R. Smith, 2005, Synthesis of industrial utility systems: cost-effective de-carbonisation, Applied Thermal Engineering, 25, 985 – 1001.*



## Existing Process Integrating Technologies (Cont.)



A typical industrial site comprises different process production units linked to a common utility system. The centralised utility system meets the demands for heat and power, creating indirect links between the processes.

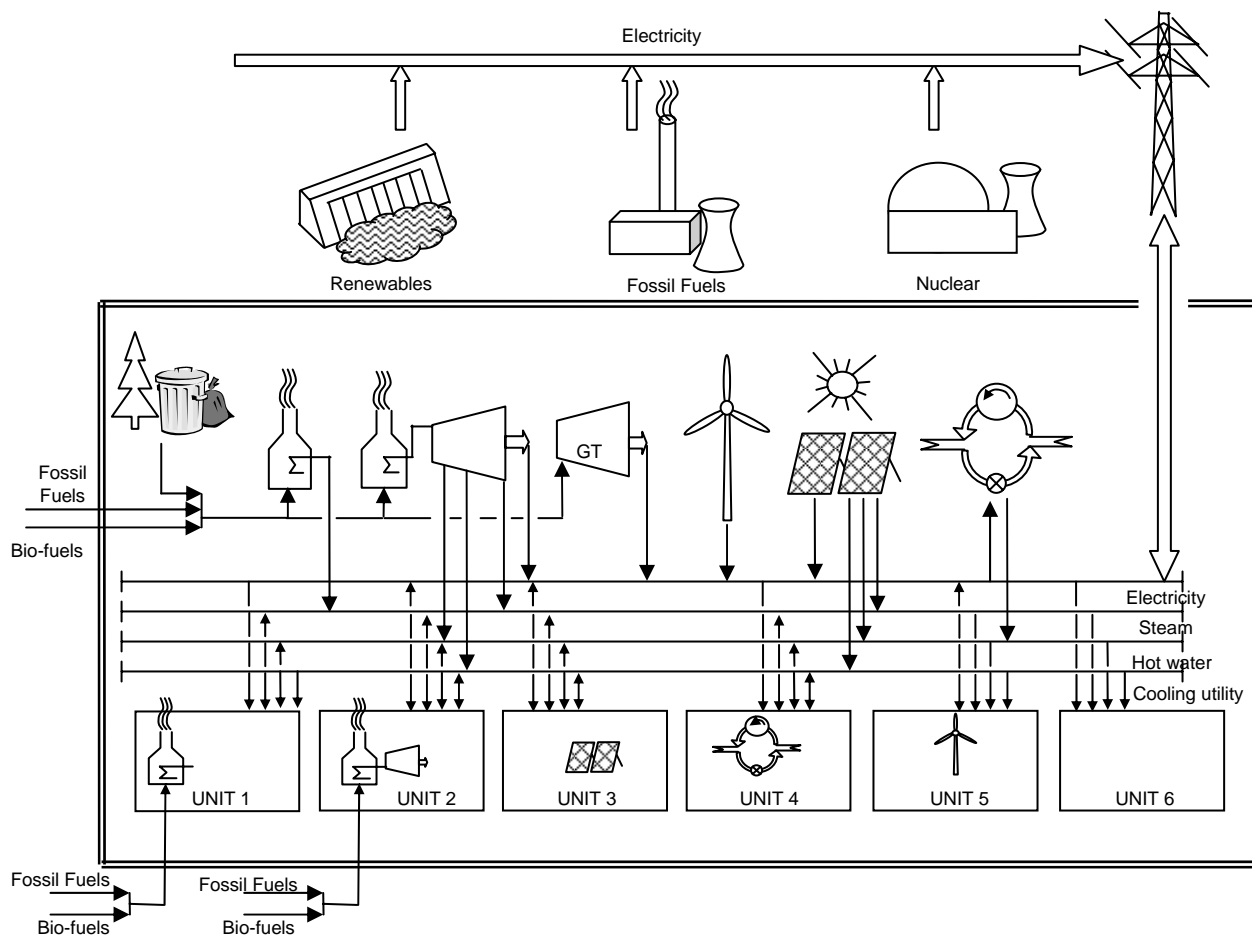


# Integrating Micro Renewable Energy Sources

The concept of an integrated energy system for the production of heat and power meeting local needs can be applied to systems involving demands produced by individual buildings and building complexes

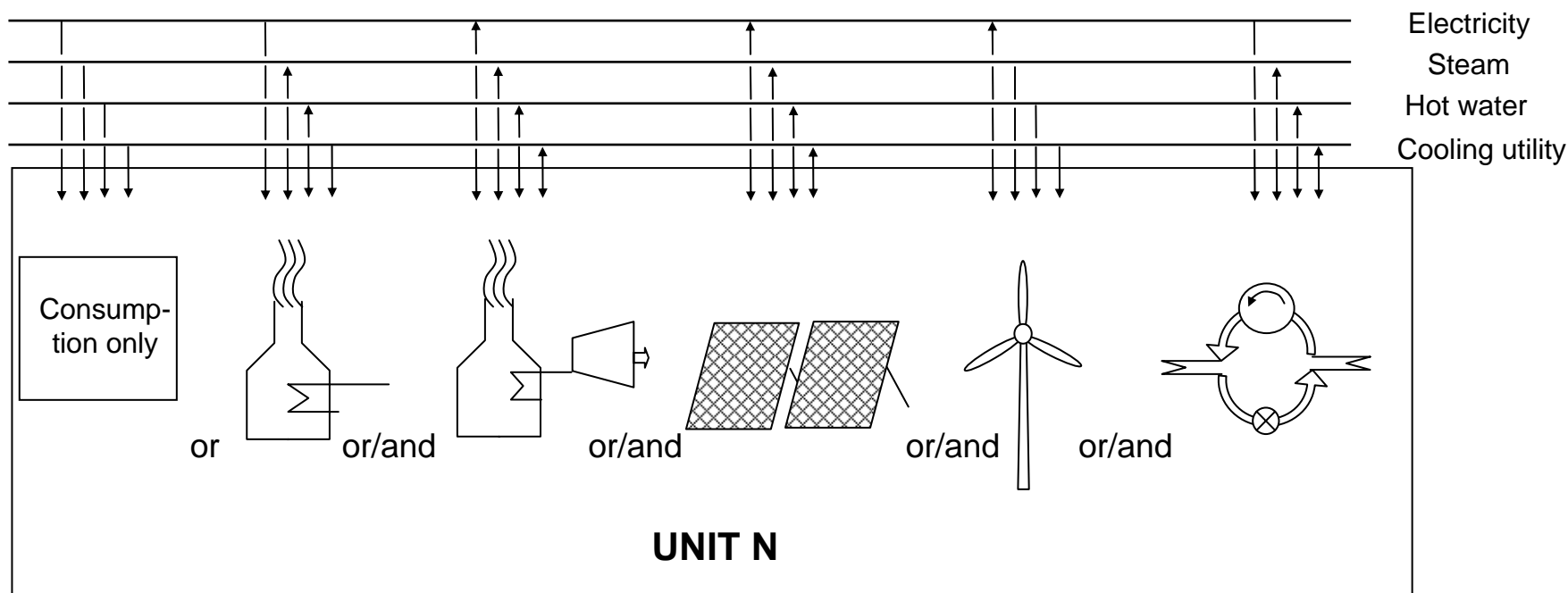


# Integrating Micro Renewable Energy Sources





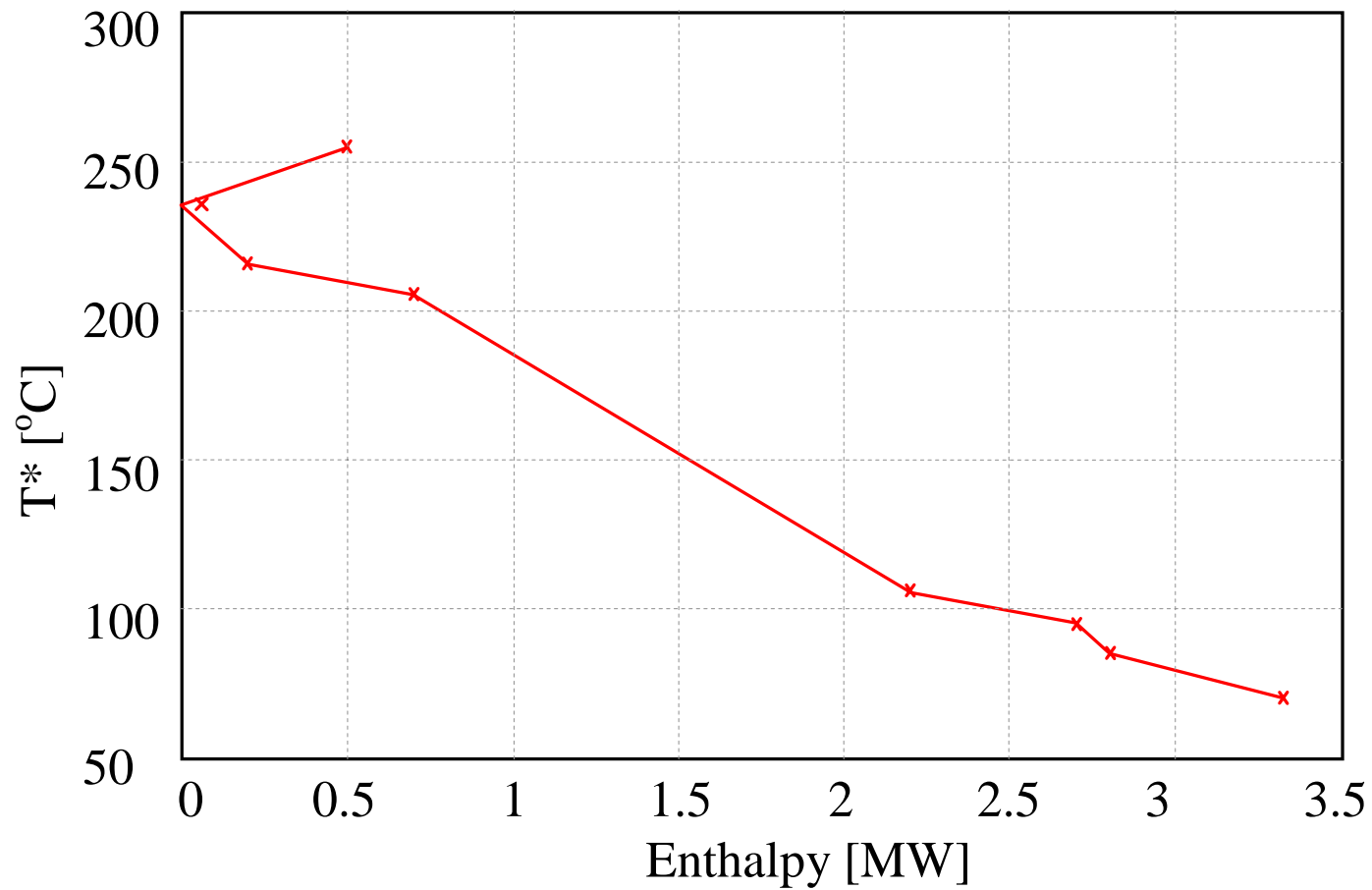
# Integrating Micro Renewable Energy Sources



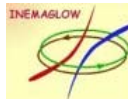
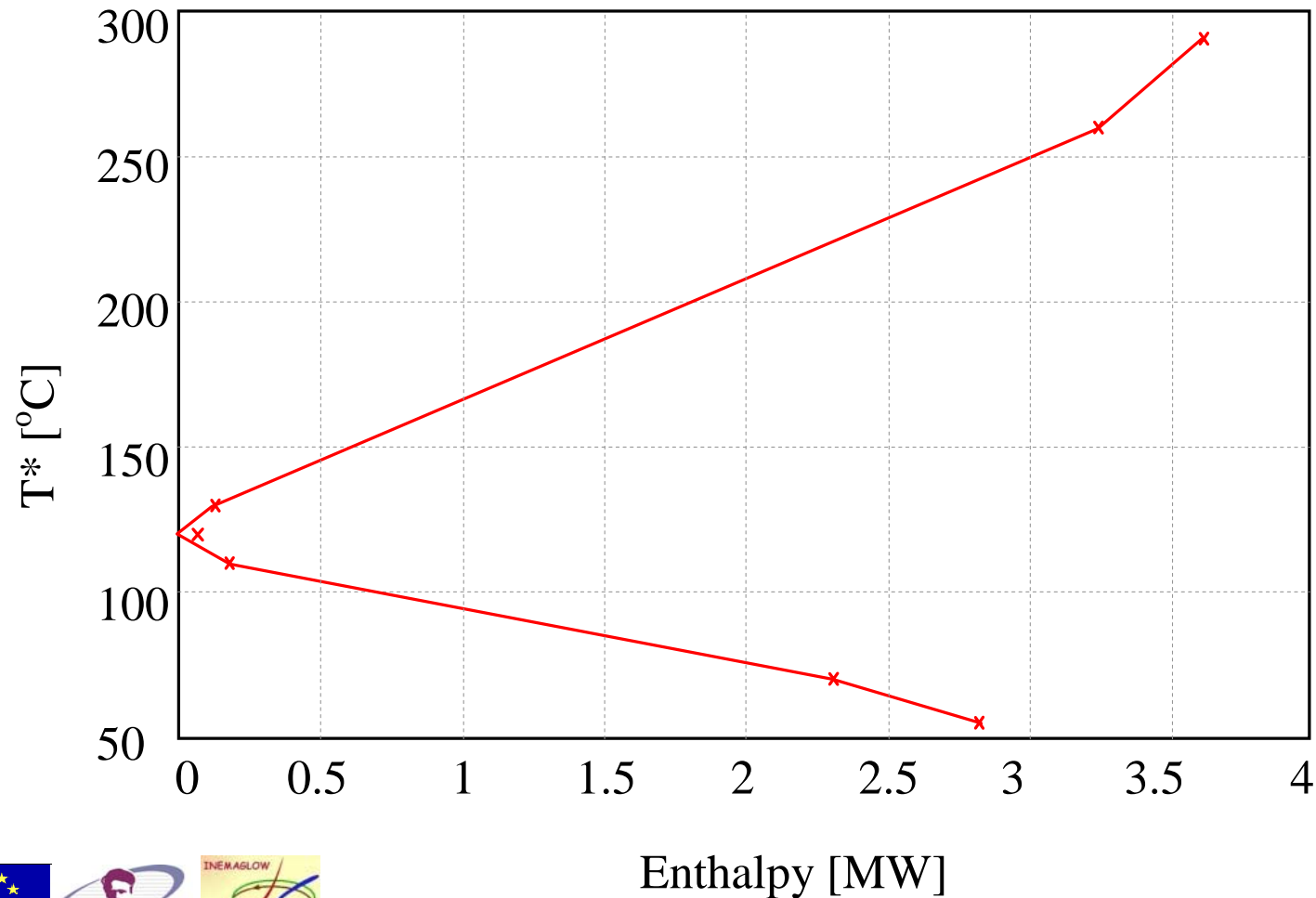
Energy consumption/generation within a unit N



# Plant 1: Grand Composite Curve with $\Delta T_{\min} = 10^\circ\text{C}$



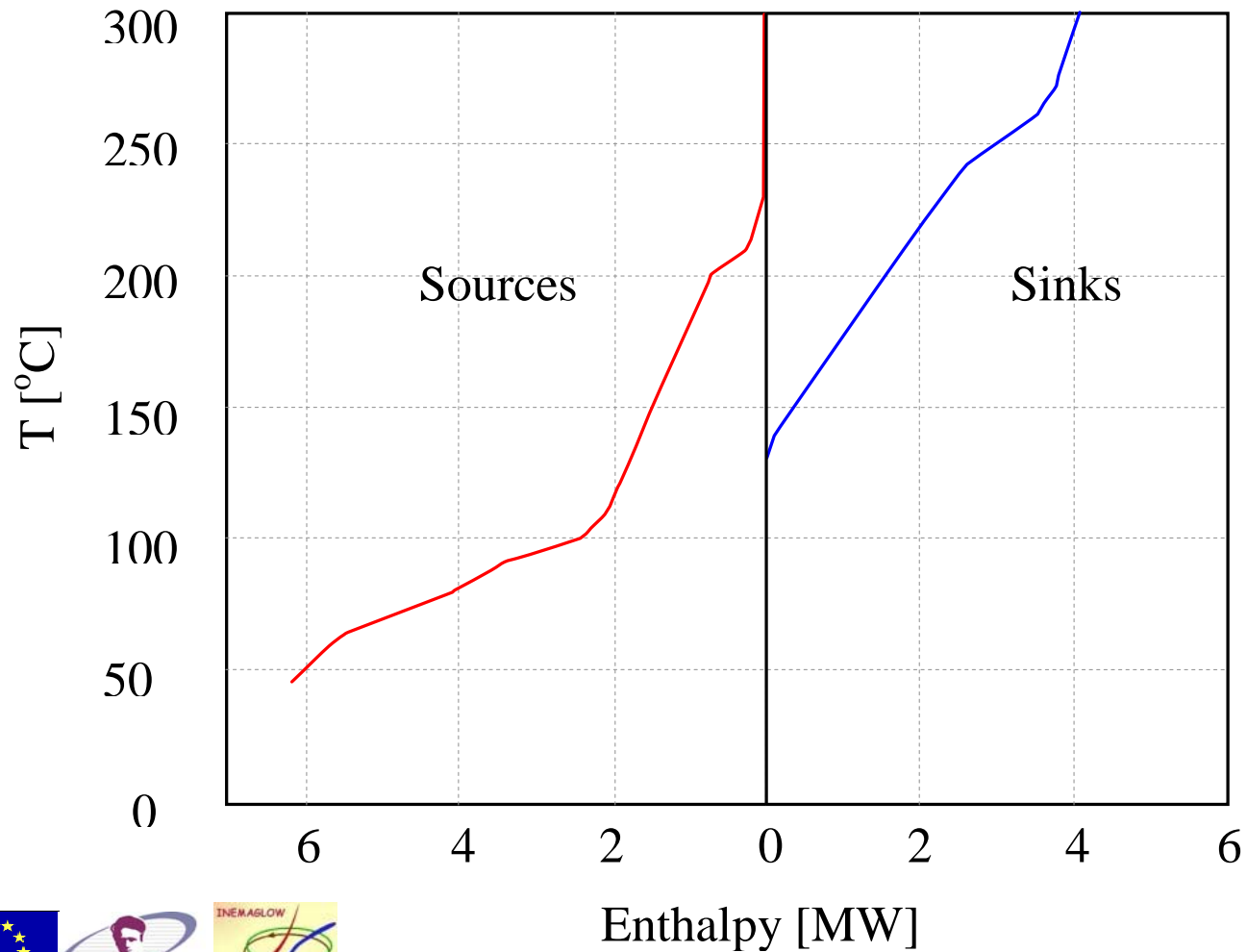
# Plant 2: Grand Composite Curve with $\Delta T_{\min} = 20^\circ\text{C}$



Enthalpy [MW]



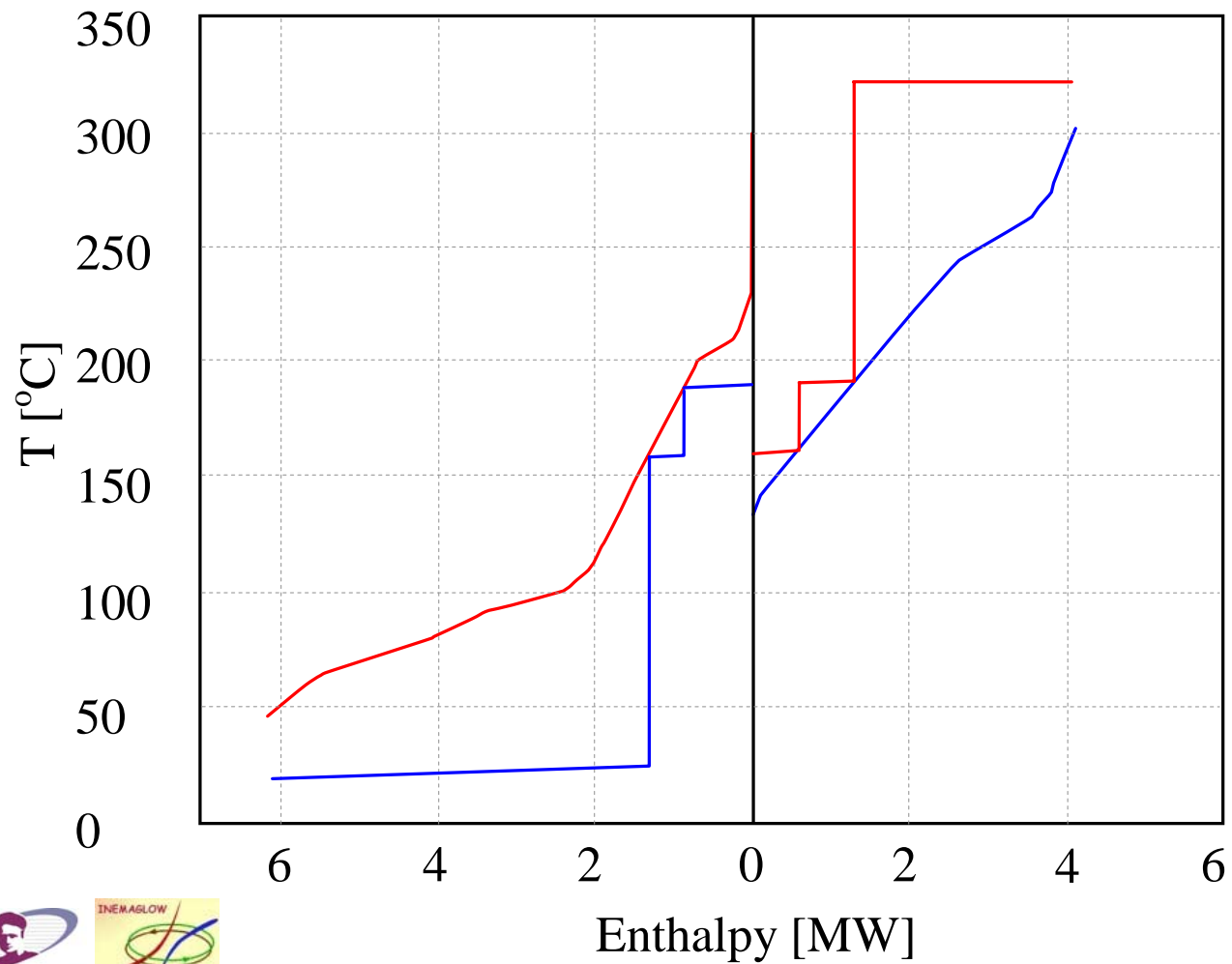
# Site Profiles



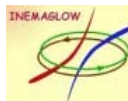
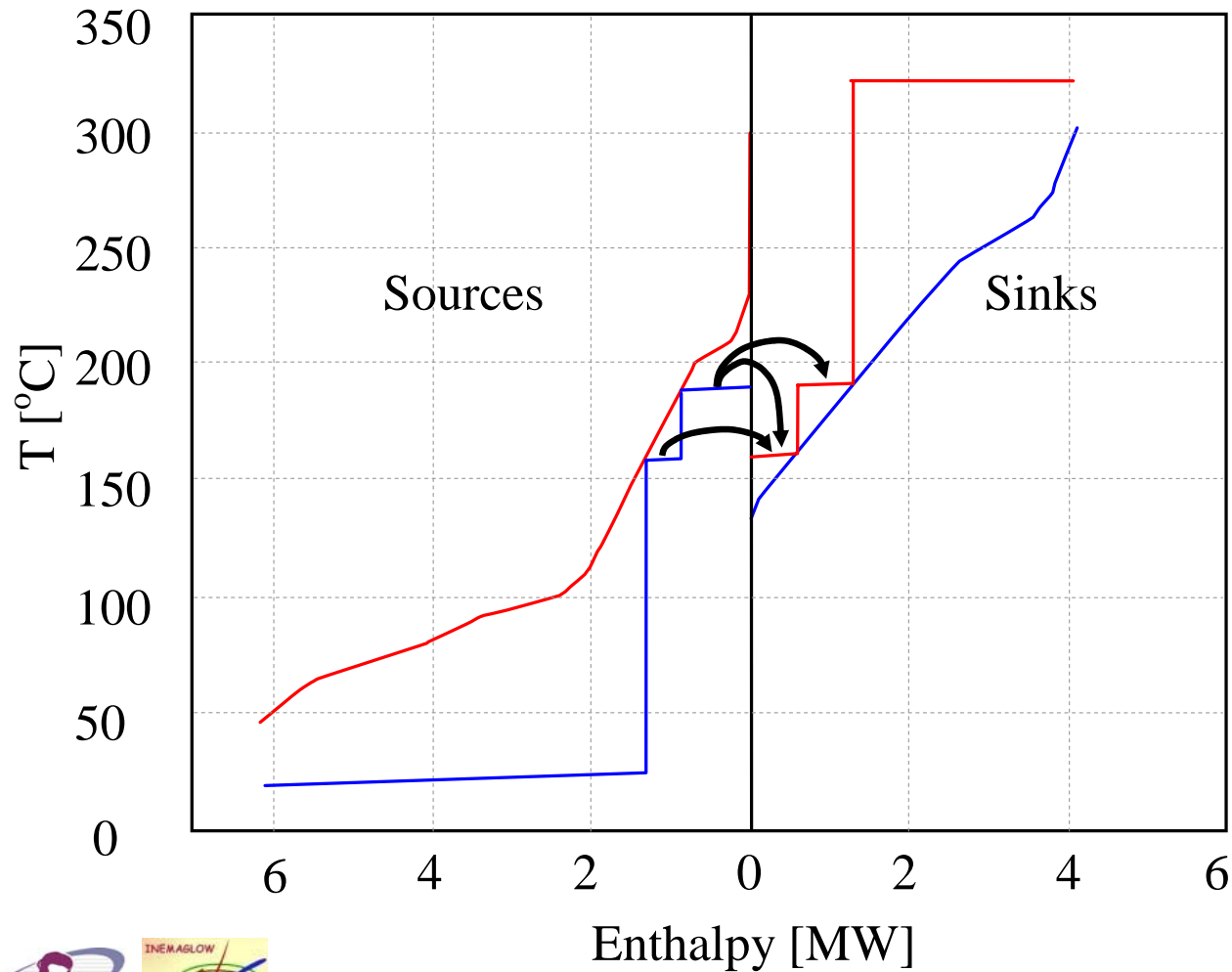
# Utilities and their parameters

| <b>Steam Main</b> | <b>Saturation Temperature [°C]</b> | <b>Used load [MW]</b> | <b>Generated Load [MW]</b> |
|-------------------|------------------------------------|-----------------------|----------------------------|
| VHP               | 320                                | 2.78                  | 0                          |
| HP                | 190                                | 0.72                  | 0.87                       |
| MP                | 160                                | 0.6                   | 0.45                       |
| CW                | 25                                 | 4.83                  | 0                          |

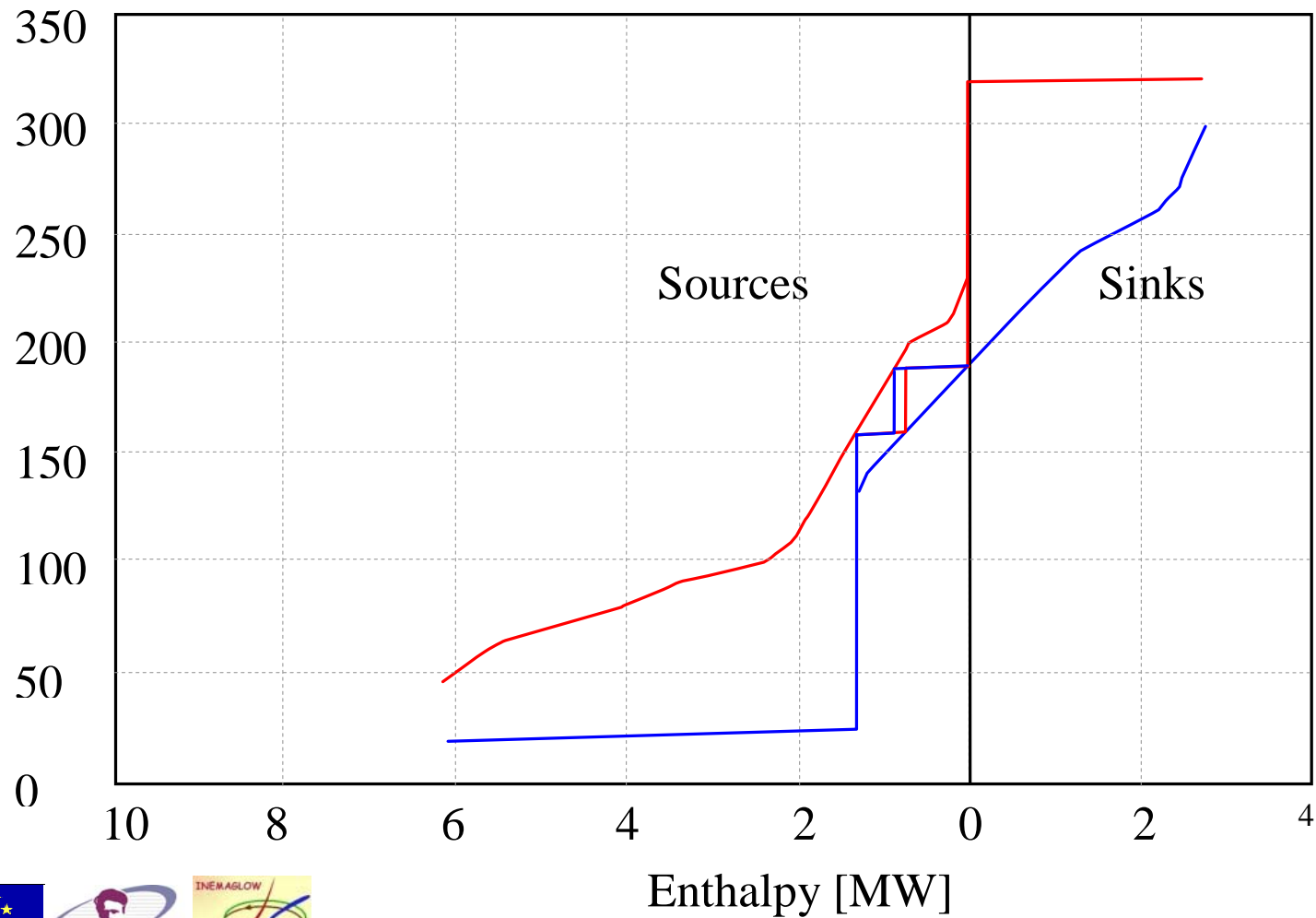
# Total Site Profiles



# Total Site Profiles with potential steam heat recovery



# Total Site Profiles with steam heat recovery



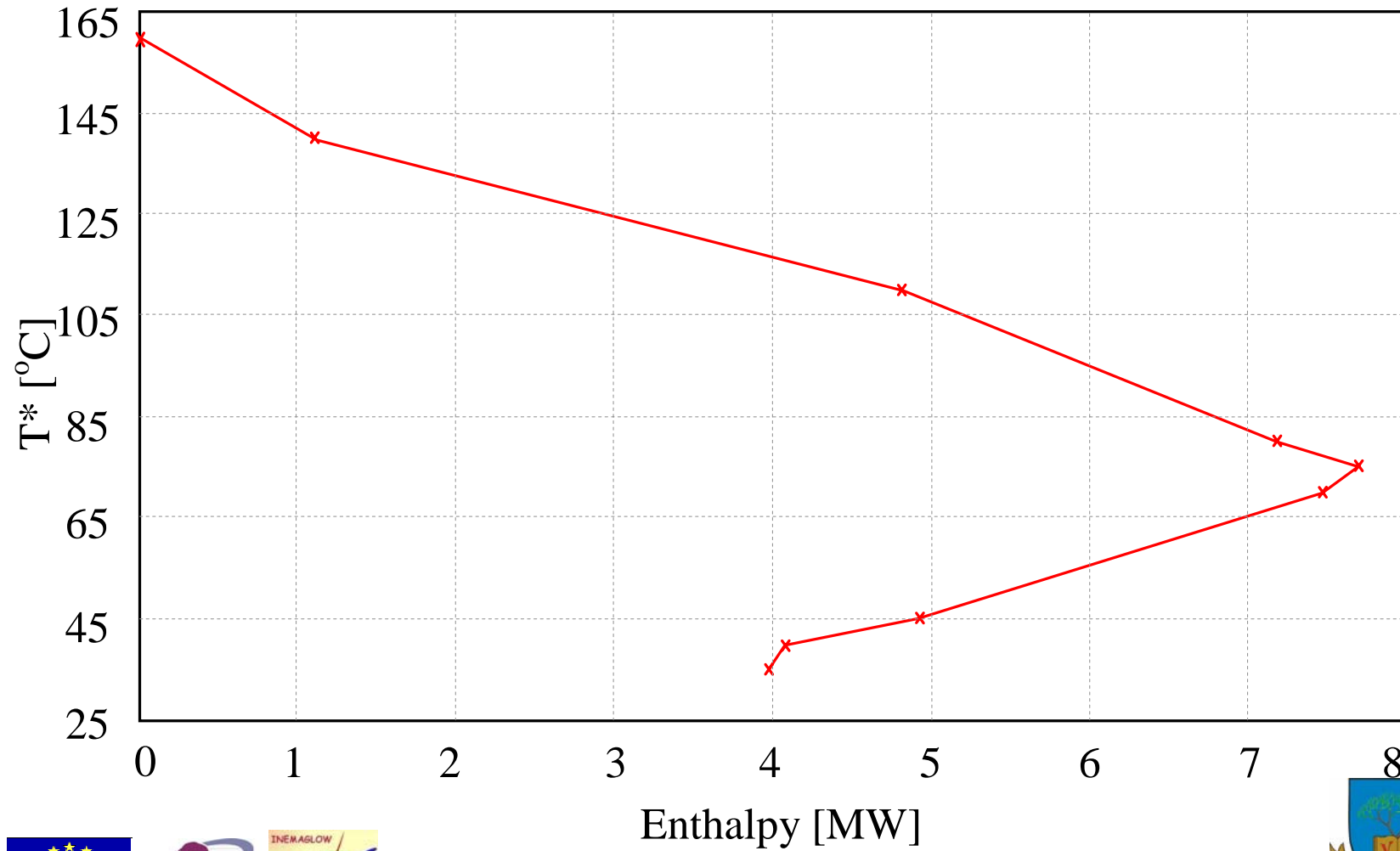


# Process plant A stream data

| Stream | Name | Tsupply [°C] | T target [°C] | DH [MW] | CP [kW/°C] |
|--------|------|--------------|---------------|---------|------------|
| 1 Hot  | A2   | 170          | 80            | 5.000   | 55.5556    |
| 2 Hot  | A1   | 150          | 55            | 6.477   | 68.1818    |
| 3 Cold | A5   | 25           | 100           | 1.500   | 20.0000    |
| 4 Cold | A6   | 70           | 100           | 0.750   | 35.0000    |
| 5 Cold | A7   | 30           | 65            | 5.250   | 150.0000   |

# Process Grand Composite

## Process Plant A ( $\Delta T_{\min} = 20 \text{ }^{\circ}\text{C}$ )

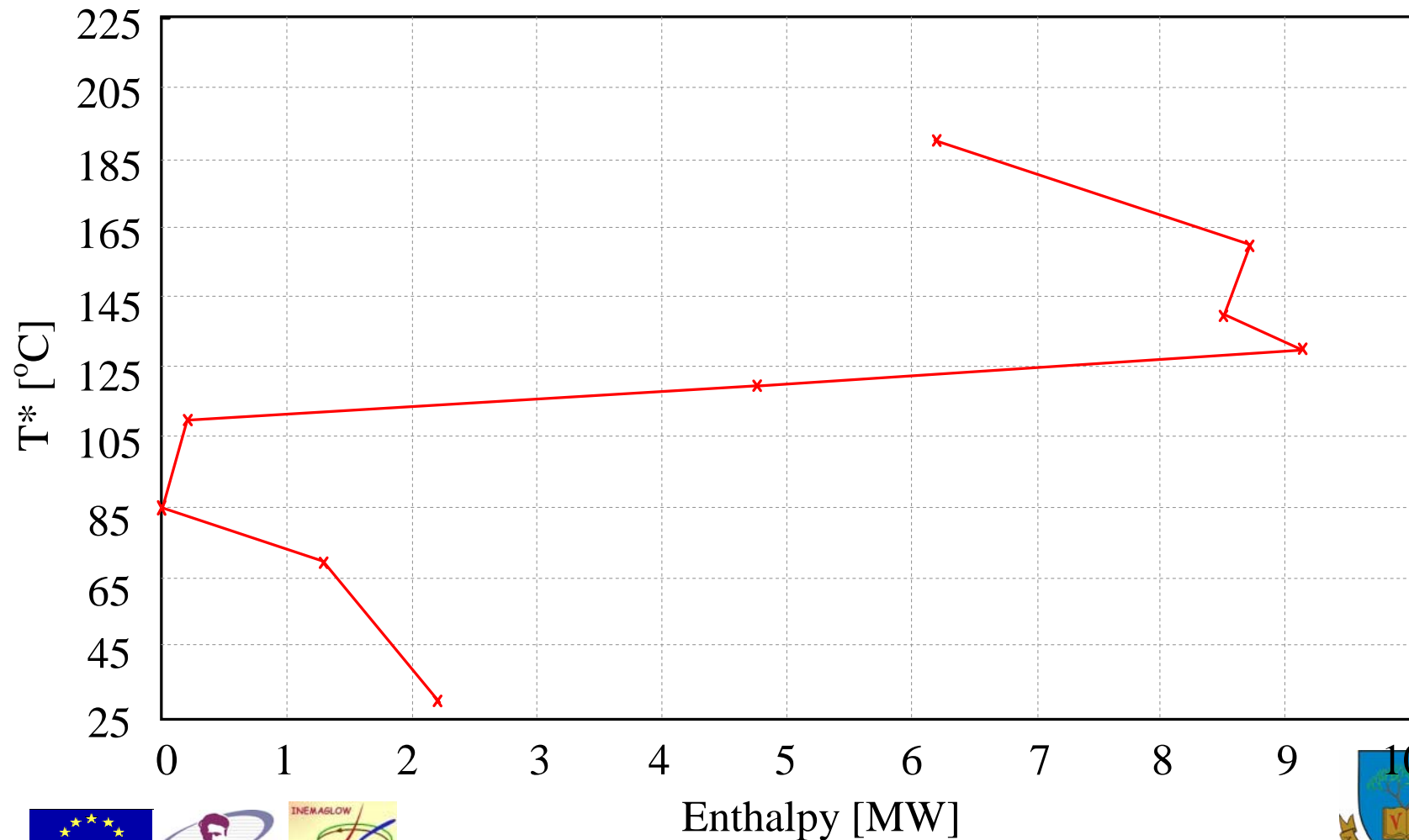


# Process plant B stream data

| Stream | Name | Tsupply [°C] | T target [°C] | DH [MW] | CP [kW/°C] |
|--------|------|--------------|---------------|---------|------------|
| 1 Hot  | B1   | 200          | 80            | 10.000  | 83.3333    |
| 2 Cold | B2   | 20           | 100           | 4.000   | 50.0000    |
| 3 Cold | B3   | 100          | 120           | 10.000  | 500.0000   |
| 4 Hot  | B4   | 150          | 40            | 8.000   | 72.7273    |
| 5 Cold | B5   | 60           | 110           | 1.000   | 20.0000    |
| 6 Cold | B6   | 75           | 150           | 7.000   | 93.3333    |

# Process Grand Composite

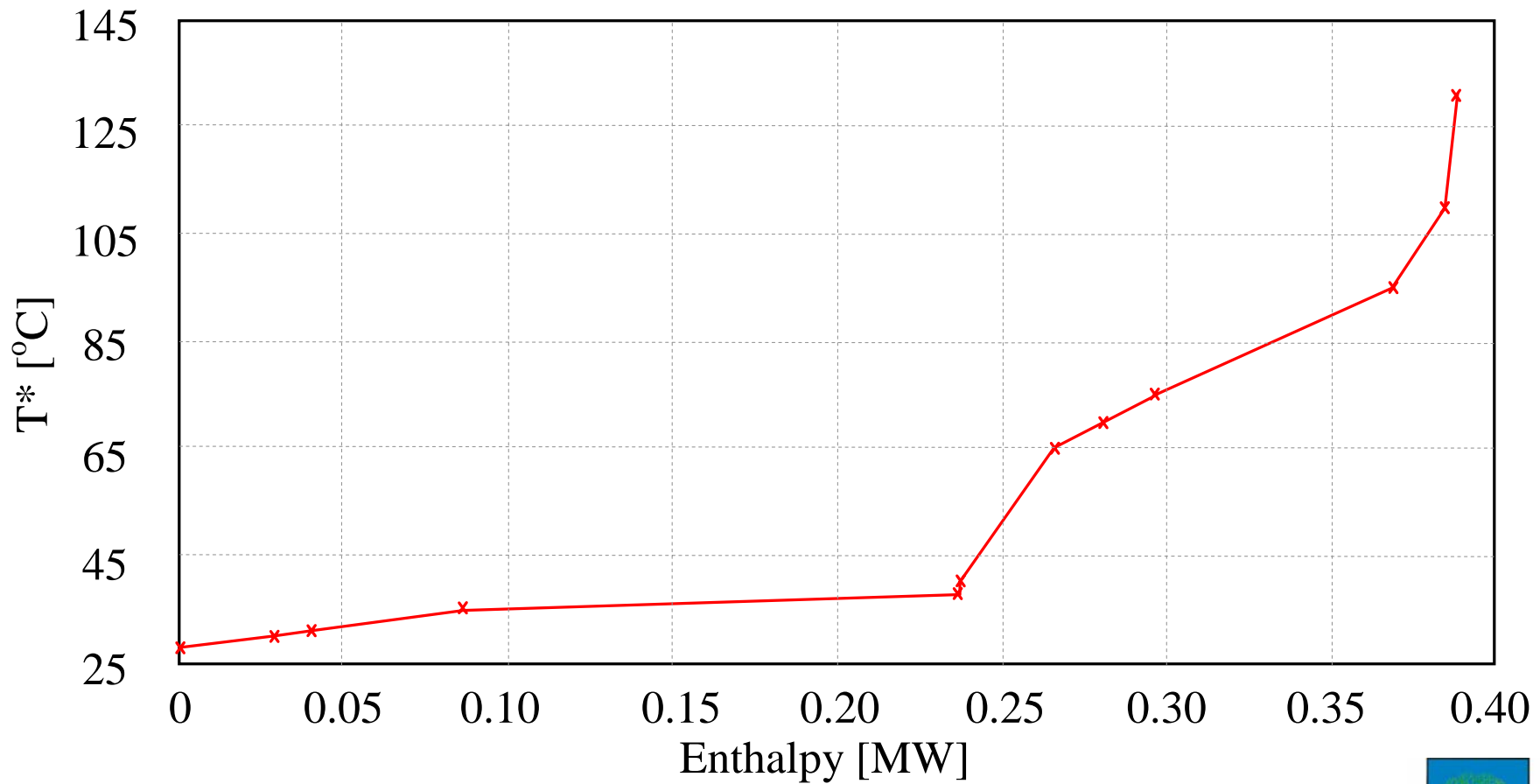
## Process Plant B ( $\Delta T_{\min} = 20 \text{ }^\circ\text{C}$ )



# Stream data of a hospital (Plant C)

| Stream  | Name                   | T supply<br>[°C] | T target<br>[°C] | DH<br>[kW] | CP<br>[kW/°C] |
|---------|------------------------|------------------|------------------|------------|---------------|
| 1 Hot   | Soapy water            | 85               | 40               | 23.85      | 0.53          |
| 2 Hot   | Condensed steam        | 80               | 40               | 96.4       | 2.41          |
| 3 Cold  | Laundry sanitary water | 25               | 55               | 17.7       | 0.59          |
| 4 Cold  | Laundry                | 55               | 85               | 77.4       | 2.58          |
| 5 Cold  | Boiler feed water      | 33               | 60               | 7.2        | 0.24          |
| 6 Cold  | Sanitary water         | 25               | 60               | 77         | 2.2           |
| 7 Cold  | Sterilization          | 30               | 121              | 12.74      | 0.14          |
| 8 Cold  | Swimming pool water    | 25               | 28               | 151.68     | 50.56         |
| 9 Cold  | Cooking                | 30               | 100              | 59.5       | 0.85          |
| 10 Cold | Heating                | 18               | 25               | 100.8      | 14.4          |
| 11 Cold | Bedpanwashers          | 21               | 121              | 5          | 0.05          |

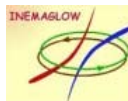
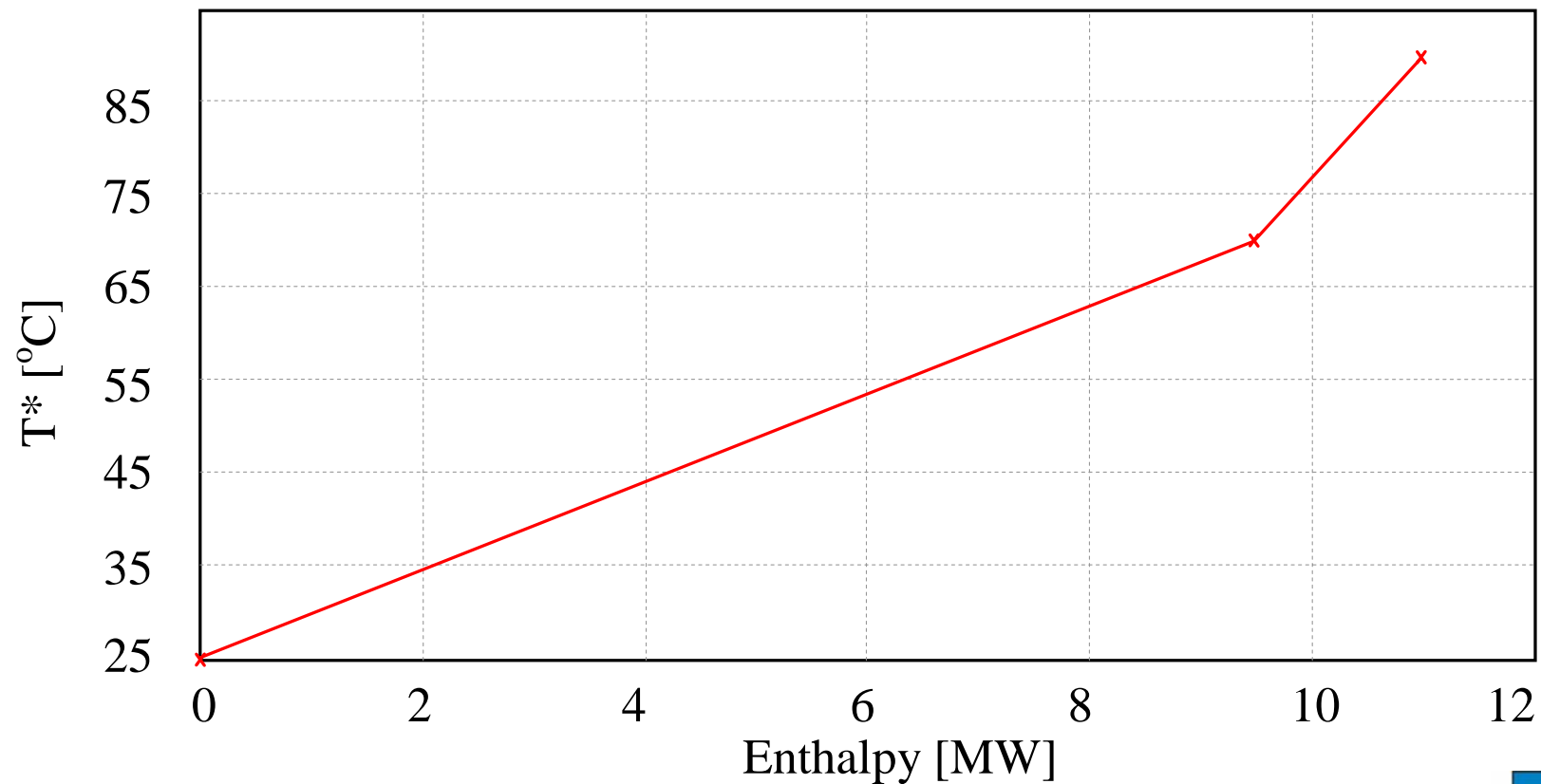
# Process Grand Composite of a hospital complex (Plant C, $\Delta T_{\min} = 20\text{ }^{\circ}\text{C}$ )



# Process Stream data of residential and office complex (Plant D)

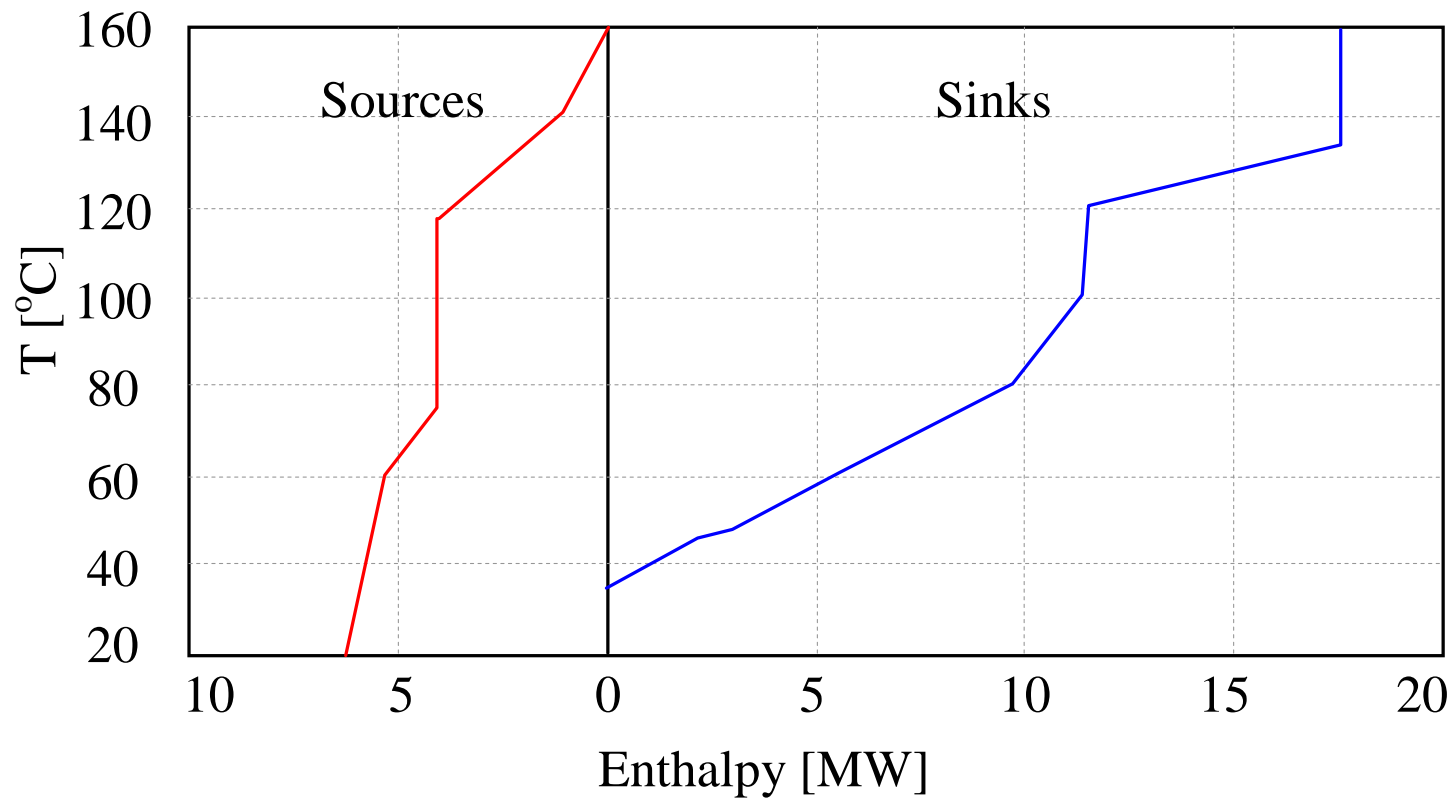
| Stream | Name             | T supply<br>[°C] | T target<br>[°C] | DH<br>[MW] | CP<br>[kW/°C] |
|--------|------------------|------------------|------------------|------------|---------------|
| 1 Hot  | District heating | 15               | 60               | 6.000      | 133.333       |
| 2 Hot  | Hot water        | 15               | 80               | 5.000      | 76.9232       |

# Process Grand Composite of residential and office complex (Plant D, $\Delta T_{\min} = 20\text{ }^{\circ}\text{C}$ )

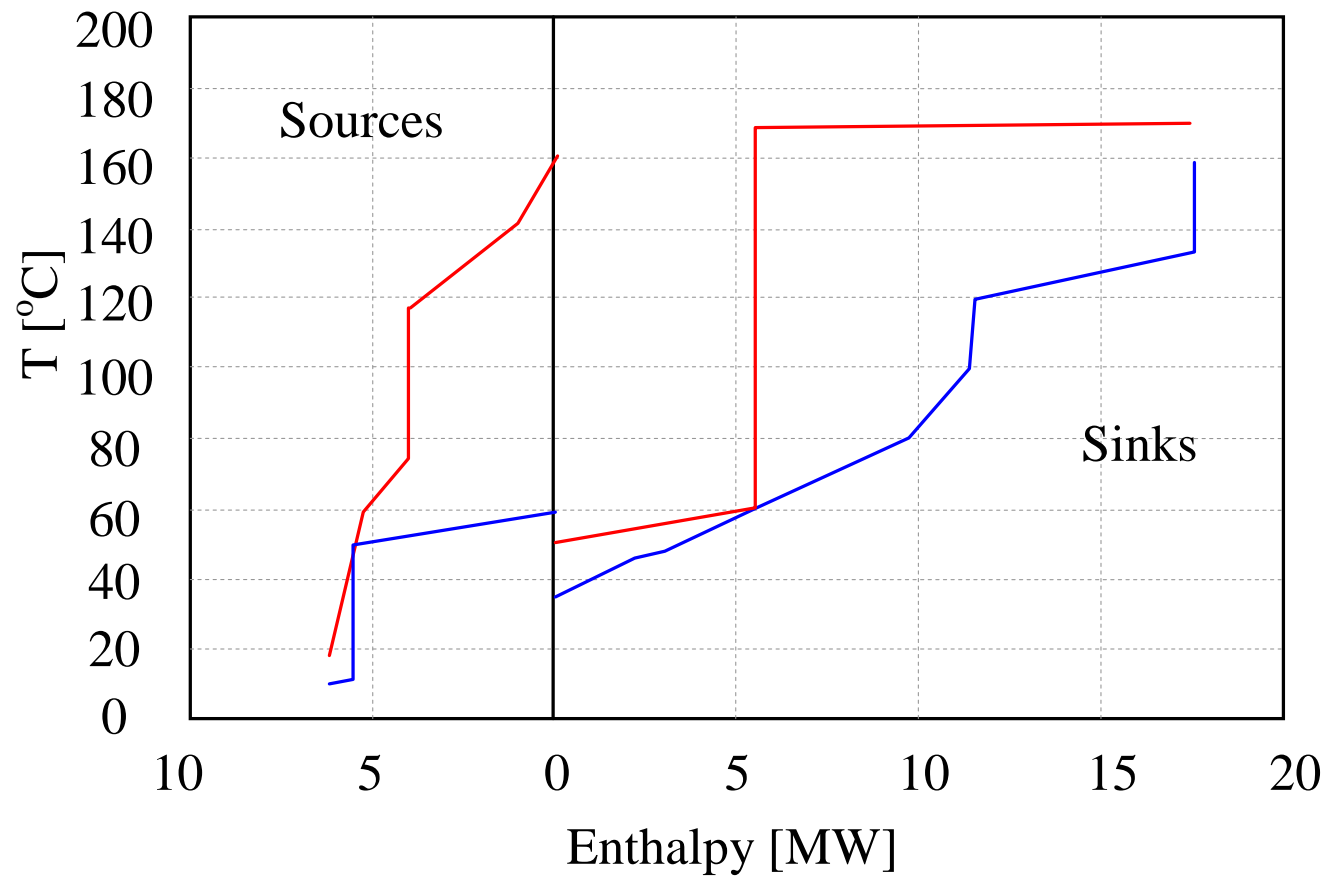




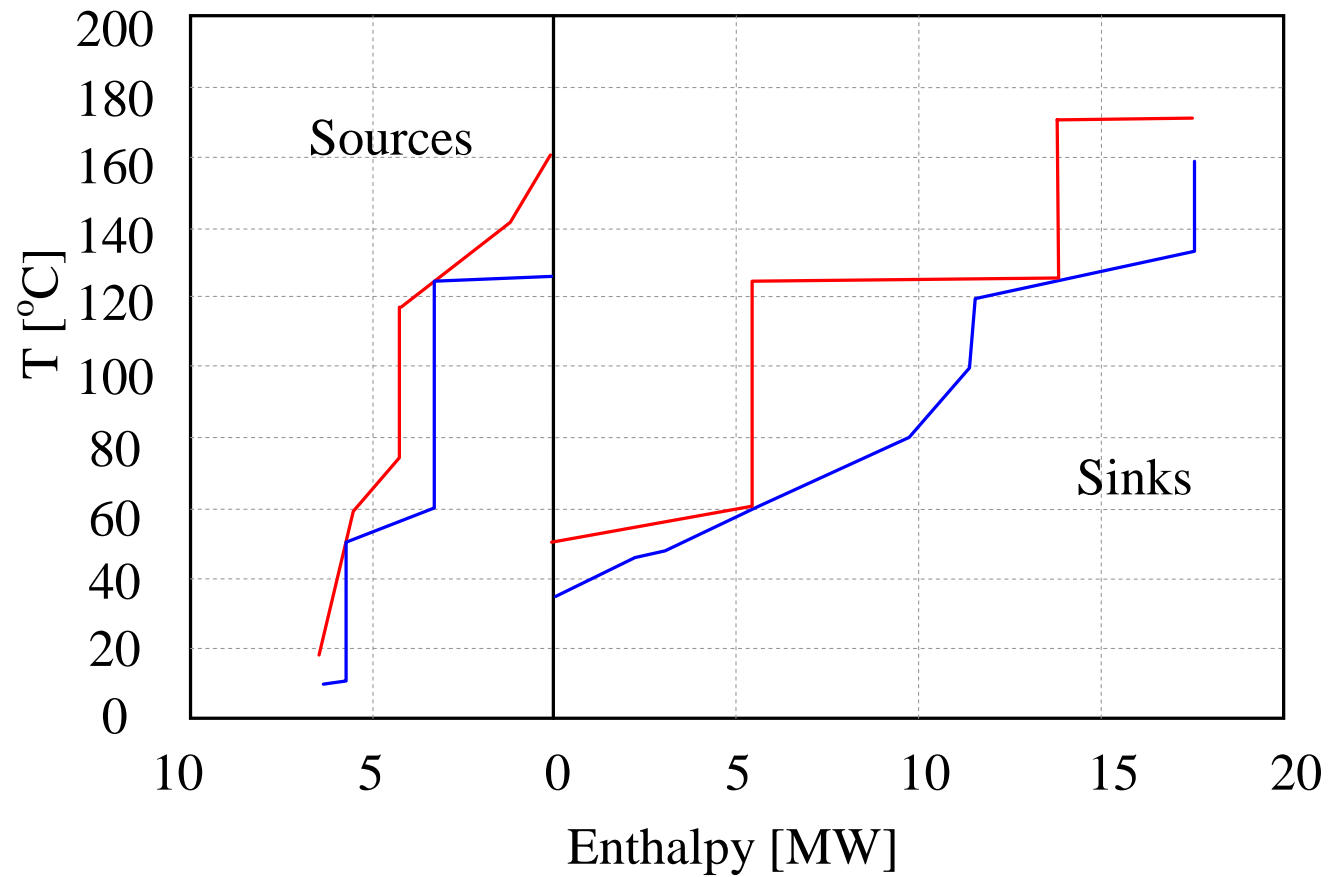
# Site Profiles



# Scenario $\alpha$ – Total Site Profiles



# Scenario $\beta$ – Total Site Profiles



## Conclusions

- Plant as well as building complexes, as individual dwellings, offices, leisure facilities, and service providers, have large energy demands in the form of electrical power and heating/cooling.
- Some of them can be met by small local renewable sources, but their CO<sub>2</sub> contribution may be larger than initially realised and better estimates can be made through the application of carbon footprints assessment



## Conclusions

- The use of integrated energy systems, including renewables, incorporating supply and demand at both the local and district level, would likely produce overall better energy efficiencies and consequently reduced emissions and carbon footprint
- The application of proven design strategies adopted from the process and energy generating industries could provide the key to successful reductions.



**More details available in**

S. Perry, J. Klemeš, I. Bulatov  
**Integrating Waste and Renewable  
Energy to reduce the Carbon Footprint of  
Locally Integrated Energy Sectors,**  
Energy 33 (10) October 2008, 1489-1497  
doi: 10.1016/j.energy.2008.03.008

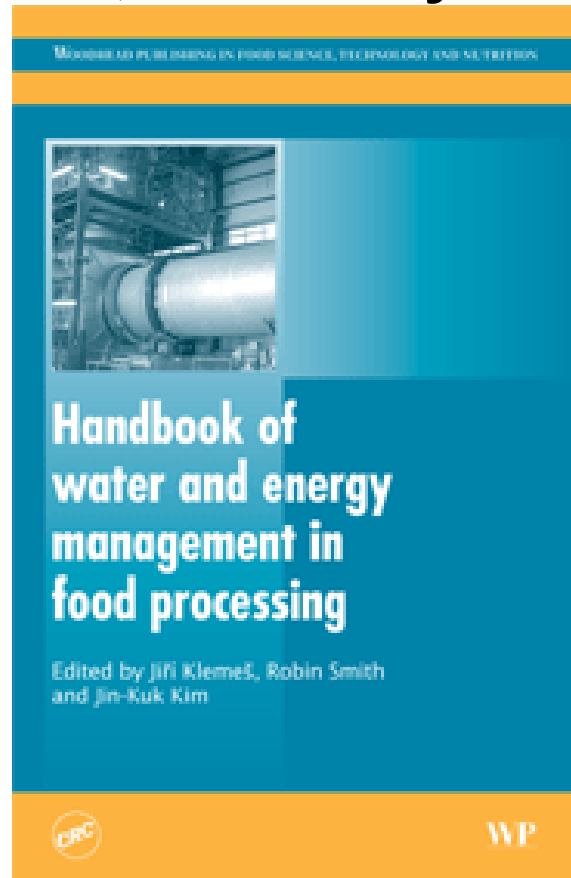


# Handbook of Water and Energy Management in Food Processing

Edited by

J Klemeš, University of Pannonia

R Smith and J-K Kim, University of Manchester, UK



# EMINET 2 Workshop

Energy for Sustainable Future



EMINENT 2 Workshop  
5 – 6 May 2008  
University of Pannonia,  
Veszprém





## Future Work

Several other footprints should be considered to provide the whole picture:

- ❖ **Water Footprint**
- ❖ **Energy Footprint**
- ❖ **Emissions Footprint**
- ❖ **Work Environment Footprint**
- ❖ .....

Let us discuss and further develop it !



## Future Work

More results are coming in

**“The Environmental Performance Strategy Map:  
an Integrated LCA approach to support the  
Strategic Decision Making Process”**

in **“Journal of Cleaner Production”**



# Acknowledgements

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